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<p>(21) International Application Number: PCT/US00/01783</p> <p>(22) International Filing Date: 21 January 2000 (21.01.00)</p> <p>(30) Priority Data:</p> <table> <tr><td>60/116,741</td><td>22 January 1999 (22.01.99)</td><td>US</td></tr> <tr><td>60/146,946</td><td>2 August 1999 (02.08.99)</td><td>US</td></tr> <tr><td>60/146,943</td><td>2 August 1999 (02.08.99)</td><td>US</td></tr> <tr><td>60/151,811</td><td>30 August 1999 (30.08.99)</td><td>US</td></tr> <tr><td>09/439,377</td><td>15 November 1999 (15.11.99)</td><td>US</td></tr> </table> <p>(63) Related by Continuation (CON) or Continuation-in-Part (CIP) to Earlier Application</p> <table> <tr><td>US</td><td>Not furnished (CON)</td></tr> <tr><td>Filed on</td><td>Not furnished</td></tr> </table> <p>(71) Applicant (<i>for all designated States except US</i>): CALIFORNIA INSTITUTE OF TECHNOLOGY [US/US]; 1200 East California Boulevard, Mail Code 201-85, Pasadena, CA 91125 (US).</p> <p>(72) Inventors; and</p> <p>(75) Inventors/Applicants (<i>for US only</i>): HAILE, Sossina, M. [US/US]; California Institute of Technology, 1200 East California Boulevard, Mail Code 138-78, Pasadena, CA</p>		60/116,741	22 January 1999 (22.01.99)	US	60/146,946	2 August 1999 (02.08.99)	US	60/146,943	2 August 1999 (02.08.99)	US	60/151,811	30 August 1999 (30.08.99)	US	09/439,377	15 November 1999 (15.11.99)	US	US	Not furnished (CON)	Filed on	Not furnished	<p>91125 (US). BOYSEN, Dane [US/US]; California Institute of Technology, 1200 East California Boulevard, Mail Code 178-38, Pasadena, CA 91125 (US). NARAYANAN, Sekharipuram, R. [US/US]; Jet Propulsion Laboratory, 1200 East California Boulevard, Mail Code 277-207, Pasadena, CA 91125 (US). CHISHOLM, Calum [US/US]; California Institute of Technology, 1200 East California Boulevard, Mail Code 198-78, Pasadena, CA 91125 (US).</p> <p>(74) Agent: HARRIS, Scott, C.; Fish & Richardson, P.C., Suite 1400, 4225 Executive Square, La Jolla, CA 92037 (US).</p> <p>(81) Designated States: AE, AL, AM, AT, AU, AZ, BA, BB, BG, BR, BY, CA, CH, CN, CR, CU, CZ, DE, DK, DM, EE, ES, FI, GB, GD, GE, GH, GM, HR, HU, ID, IL, IN, IS, JP, KE, KG, KP, KR, KZ, LC, LK, LR, LS, LT, LU, LV, MA, MD, MG, MK, MN, MW, MX, NO, NZ, PL, PT, RO, RU, SD, SE, SG, SI, SK, SL, TJ, TM, TR, TT, TZ, UA, UG, US, UZ, VN, YU, ZA, ZW, ARIPO patent (GH, GM, KE, LS, MW, SD, SL, SZ, TZ, UG, ZW), Eurasian patent (AM, AZ, BY, KG, KZ, MD, RU, TJ, TM), European patent (AT, BE, CH, CY, DE, DK, ES, FI, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE), OAPI patent (BF, BJ, CF, CG, CI, CM, GA, GN, GW, ML, MR, NE, SN, TD, TG).</p> <p>Published <i>Without international search report and to be republished upon receipt of that report.</i></p>	
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<p>(54) Title: PROTON CONDUCTING MEMBRANE USING A SOLID ACID</p> <p>(57) Abstract</p> <p>A solid acid material is used as a proton conducting membrane in an electrochemical device. The solid acid material can be one of a plurality of different kinds of materials. A binder can be added, and that binder can be either a nonconducting or a conducting binder. Nonconducting binders can be, for example, a polymer or a glass. A conducting binder enables the device to be both proton conducting and electron conducting.</p>																						

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PROTON CONDUCTING MEMBRANE USING A SOLID ACIDCross-Reference To Related Applications

5 This application claims benefit of U.S. Provisional Applications, serial number 60/116,741, filed January 22, 1999; serial number 60/146,946, filed August 2, 1999; serial number 60/146,943, filed August 2, 1999 and serial number 60/151,811, filed August 30, 1999.

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Statement As To Federally-Sponsored Research

The invention described herein was made in the performance of work under a NASA contract, and is subject to the provisions of Public Law 96-517 (U.S.C. 202) in which the Contractor has
15 elected to retain title.

Field

The present application describes a proton conducting membrane formed using an solid acid in its solid phase. More 5 specifically, the present application teaches a proton conducting membrane, formed using an solid acid mixed with a supporting binder material, that is impermeable to fluids such as gas and water, can operate without hydration, and has high proton conductivity.

10

Background

Proton conducting materials have a number of applications. Proton conducting membranes are widely utilized in devices which use a chemical reaction to produce or store electricity, or use 15 electricity to drive a chemical process. Materials which conduct both protons and electrons ("mixed proton and electron conductors") are utilized in related applications.

Electrochemical devices depend on the flow of protons, or the flow of both protons and electrons through a proton conducting membrane. Exemplary electrochemical devices include a fuel cell, an electrolysis cell, a hydrogen separation cell, a 5 battery, a supercapacitor, and a membrane reactor. There are other electrochemical devices which also use a proton conducting membrane.

An important use for proton conducting membranes is in fuel cells. Fuel cells are attractive alternatives to combustion 10 engines for the generation of electricity because of their higher efficiency and the lower level of pollutants they produce. A fuel cell generates electricity from the electrochemical reaction of a fuel e.g. methane, methanol, gasoline, or hydrogen, with oxygen normally obtained from air.

15 There are three common types of fuel cells used at temperatures close to ambient. A direct hydrogen/air fuel cell system stores hydrogen and then delivers it to the fuel cell as needed.

In an indirect hydrogen/air fuel cell, hydrogen is 20 generated on site from a hydrocarbon fuel, cleaned it of carbon monoxide (CO), and subsequently fed to the fuel cell.

A direct methanol fuel cell ("DMFC"), feeds methanol/water solution directly to the fuel cell, e.g., without any fuel

processing. One type of DMFC has been described, for example, in U.S. Patent No. 5,559,638. There are various advantages and disadvantages inherent within all three configurations. All are, to a greater or lesser extent, limited by the performance of the 5 proton conducting membrane.

Nafion™, a perfluorinated sulphonic acid polymer, is often used as a membrane material for fuel cells which operate at temperatures close to ambient. Other hydrated polymers have also been used as proton conductive materials. Membranes of modified 10 perfluorinated sulfonic acid polymers, polyhydrocarbon sulfonic acid polymers, and composites thereof are also known. These and related polymers are used in hydrated form. Proton transport occurs by the motion of hydronium ions, H_3O^+ . Water is necessary in order to facilitate proton conduction. Loss of water 15 immediately results in degradation of the conductivity. Moreover, this degradation is irreversible - a simple reintroduction of water to the system does not restore the conductivity. Thus, the electrolyte membranes of these hydrated polymer-based fuel cells must be kept humidified during 20 operation. This introduces a host of balance-of-plant needs for water recirculation and temperature control.

- A second limitation derives from the need to maintain water in the membrane. In order to maintain hydration, the temperature of operation cannot exceed 100°C without cell pressurization.
- High temperature operation could be desirable, however, to
- 5 increase catalyst efficiency in generating protons at the anode (in both H₂ and direct methanol fuel cells) and to improve catalyst tolerance to carbon monoxide ("CO"). CO is often present in the fuel that is used in the fuel cells. The CO can poison the precious metal catalysts. This is particularly
- 10 problematic in indirect hydrogen/air fuel cells for which hydrogen is generated on site. High temperatures also benefit the reduction reaction on the cathode.
- Another limitation of hydrated polymer electrolytes occurs in applications in methanol fuel cells. These polymers can be
- 15 permeable to methanol. Direct transport of the fuel (i.e. methanol) across the membrane to the air cathode results in losses in efficiency.
- Alternate proton conducting materials, which do not require humidification, which can be operated at slightly elevated
- 20 temperatures, and/or which are impermeable to methanol, are desirable for fuel cell applications.

In the field of hydrogen separation, a proton conducting membrane is utilized to separate hydrogen from other gases such as CO and/or CO₂. Palladium is often used for this application.

Palladium is permeable to molecular hydrogen, but not in general
5 to other gases. There are drawbacks to the use of this material. It is expensive and the hydrogen diffusion rate is low. It would be desirable to develop new materials which are less expensive and exhibit higher proton/hydrogen transport rates.

In general, materials utilized in other electrochemical
10 devices such as electrolysis cells, batteries, supercapacitors, etc., include liquid acid electrolytes, which are highly corrosive, and solid polymer proton conductors, which require humidification or exhibit insufficient proton conductivity. High conductivity, high chemical and thermal stability solid membranes
15 with good mechanical properties are desirable for all of these applications.

Summary

The present specification defines a new kind of material for
20 a proton conducting membrane. Specifically, a proton conducting material is formed using an solid acid. The solid acid can be of the general form M_aH_b(XO_t)_c or M_aH_b(XO_t)_c·nH₂O,
where:

M is one or more of the species in the group consisting of Li, Be, Na, Mg, K, Ca, Rb, Sr, Cs, Ba, Tl and NH₄⁺ or Cu⁺;

X is one or more of the species in the group consisting of Si, P, S, As, Se, Te, Cr and Mn; and

5 a, b, c, n and t are rational numbers.

Solid acids do not rely on the presence of hydronium ions for proton transport, thus they do not require hydration for use as proton conductors.

A preferred solid acid used according to this specification
10 is a solid phase solid acid that exhibits a superprotic phase, a phase in which the solid has disorder in its crystal structure and a very high proton conductivity.

An embodiment uses a structural binder or matrix material to enhance the mechanical integrity and/or chemical stability of the
15 membrane. That structural binder can be many different kinds of materials in the different embodiments. In particular, the structural binder can be a polymer, a ceramic, or an oxide glass.

Another embodiment uses an electronically conducting material as a matrix. This creates a membrane which conducts
20 both protons and electrons.

The resulting material can be used for a proton conducting material in a device that relies on the flow of protons or the flow of both protons and electrons across a membrane, herein an "electrochemical" device e.g. a fuel cell, a hydrogen separation 5 membrane, or a electrolysis cell.

Brief Description of the Drawings

Figure 1 shows an exemplary hydrogen/air fuel cell using an solid acid supported by a binder as its proton conducting 10 membrane.

Figure 2 shows an exemplary direct methanol fuel cell using an solid acid supported by a binder as its proton conducting membrane

Figure 3 shows a hydrogen separation membrane for the 15 removal of CO and other gases from hydrogen;

Figure 4 shows another type of hydrogen separation membrane made of a proton conducting composite; and

Figures 5 and 6 show a membrane reactor.

20

Detailed Description

The present application teaches using an solid acid as a proton conducting membrane.

A solid acid can be of the general form $M_aH_b(XO_t)_c \cdot nH_2O$,

where:

M is one or more of the species in the group consisting of Li, Be, Na, Mg, K, Ca, Rb, Sr, Cs, Ba, Tl and NH₄⁺;

X is one or more of the species in the group consisting of
5 Si, P, S, As, Se, Te, Cr and Mn; and

a, b, c, n and t are rational numbers; with t preferably being 3 or 4, and where t≥0..

The solid acids used herein are compounds, such as CsHSO₄, whose properties are intermediate between those of a normal acid, 10 such as H₂SO₄, and a normal salt, such as Cs₂SO₄. In general, the chemical formula of the solid acids of the type used according to the present specification can be written as a combination of the salt and the acid.

In general, solid acids are comprised of oxyanions, for 15 example SO₄, SO₃, SeO₄, SeO₃, SiO₄, PO₄ or AsO₄, etc., which are linked together via O-H.... O hydrogen bonds. The structure may contain more than one type of XO₄ or XO₃ group, and may also contain more than one type of M species.

Certain solid acids are solid materials at room temperature.

Many different solid acids are contemplated by this specification. One example of a material that can be used as the solid acid is CsHSO₄, which is intermediate between Cs₂SO₄ (a normal salt) and H₂SO₄ (a normal acid). In this case, the solid acid can be written as 0.5 Cs₂SO₄ * 0.5 H₂SO₄. Another example, using the same salt and the same acid, is 1.5 Cs₂SO₄ * 0.5 H₂SO₄, to give Cs₃H(SO₄)₂.

Other examples are:

CsH₂PO₄, Cs₅(HSO₄)₃(H₂PO₄)₂, Cs₂(HSO₄)(H₂PO₄), Cs₃(HSO₄)₂(H₂PO₄),
10 Cs₃(HSO₄)₂(H_{1.5}(S_{0.5}P_{0.5})O₄), Cs₅H₃(SO₄)₄·xH₂O, TlHSO₄, CsHSeO₄,
Cs₂(HSeO₄)(H₂PO₄), Cs₃H(SeO₄)₂ (NH₄)₃H(SO₄)₂, (NH₄)₂(HSO₄)(H₂PO₄),
Rb₃H(SO₄)₂, Rb₃H(SeO₄)₂, Cs_{1.5}Li_{1.5}H(SO₄)₂, Cs₂Na(HSO₄)₃, TlH₃(SeO₃)₂,
CsH₂AsO₄ (NH₄)₂(HSO₄)(H₂AsO₄), CaNaHSiO₄

The preferred material for any specific electrochemical device depends on the application. For example, Cs₂(HSO₄)(H₂PO₄) may be preferred for electrochemical devices where high conductivity is critical. (NH₄)₃H(SO₄)₂ may be preferred where low cost is critical. CaNaHSiO₄ may be preferred where chemical stability is critical.

Solid acids have certain characteristics that can be advantageous when used as a proton conducting membrane. The proton transport process does not rely on the motion of hydronium ions, thus solid acids need not be humidified and their conductivity is substantially independent of humidity. Another advantage is that solid acids are generally stable against thermal decomposition at elevated temperatures. The thermal decomposition temperature for some of the solid acids described in this specification, e.g., CaNaHSiO₄, can be as high as 350°C.

Since solid acids need not be humidified, solid acid based membranes can be operated at elevated temperatures, e.g. temperatures above 100°C.

The conductivity of solid acids may be made purely protonic, or both electronic and protonic depending on the choice of the X element in the chemical formula M_aH_b(XO₄)_c·nH₂O or M_aH_b(XO₃)_c·nH₂O. That is, by using a given amount of a variable valence element such as Cr or Mn for X, the solid acid can be made to conduct electrons as well as protons.

Another advantage is caused by the structure of the solid acids themselves. Since solid acids are dense, inorganic materials, they are impermeable to gases and other fluids that may be present in the electrochemical environment, e.g., gases and hydrocarbon liquids.

The materials are also relatively inexpensive.

This combination of properties: good conductivity in dry environments, conductivity which can be controlled to be either purely proton conducting or both electron and proton conducting, impermeability to gases and hydrocarbon liquids, serviceability at elevated temperatures, e.g. temperatures over 100°C and relatively low cost, render solid acids as useful materials for use as membranes in electrochemical devices.

Solid acids exhibit another advantageous property for applications in proton conducting membranes. Under certain conditions of temperature and pressure, the crystal structure of a solid acid can become disordered. Concomitant with this disorder is an high conductivity, as high as 10^{-3} to $10^{-2} \Omega^{-1}\text{cm}^{-1}$.

Because of the high proton conductivity of the structurally disordered state, it is known as a superprotic phase. The proton transport is believed to be facilitated by rapid XO_4 or XO_3 group reorientations, which occur because of the disorder.

Many solid acids enter a superprotic state at a temperature between 50 and 150°C at ambient pressures. The transition into the superprotic phase may be either sharp or gradual. The superprotic phase is marked by an increase in 5 conductivity, often by several orders of magnitude. At temperatures above the transition temperature, the solid acid is superprotic and retains its high proton conductivity until the decomposition or melting temperature is reached.

Solid acids that undergo a superprotic transition include:
10 CsHSO_4 , $\text{Cs}_2(\text{HSO}_4)(\text{H}_2\text{PO}_4)$, $\text{Cs}_3(\text{HSO}_4)_2(\text{H}_2\text{PO}_4)$,
 $\text{Cs}_3(\text{HSO}_4)_2(\text{H}_{1.5}(\text{S}_{0.5}\text{P}_{0.5})\text{O}_4)$, $\text{Cs}_5\text{H}_3(\text{SO}_4)_4 \cdot x\text{H}_2\text{O}$, CsHSeO_4 , $\text{Cs}_3\text{H}(\text{SeO}_4)_2$,
 $(\text{NH}_4)_3\text{H}(\text{SO}_4)_2$, $\text{Rb}_3\text{H}(\text{SeO}_4)_2$.

The superprotic phases of solid acids have increased conductivity. An interesting embodiment is a solid acid operated 15 at a temperature above the superprotic transition temperature, and below the decomposition or melt temperature.

Despite the many advantageous properties of solid acids, problems can be encountered in trying to implement them in electrochemical devices because many solid acids are water 20 soluble. They can also be difficult to process into large area membranes, and they often have poor mechanical properties. Some solid acids, such as CaNaHSiO_4 and other silicates, are not soluble in water.

Because of these difficulties, a disclosed embodiment includes a composite comprised of an solid acid embedded in a supporting matrix. The solid acid part of the composite provides the desired electrochemical activity, whereas the matrix provides 5 mechanical support and also may increase chemical stability. Different materials are contemplated herein for use as the supporting matrix.

In light of the properties of solid acids outlined above, the preferred embodiment is a composite material comprised of a 10 solid acid embedded in a supporting matrix and operated at a slightly elevated temperature. In such a composite, the solid acid is in its superprotomic phase, exhibits high conductivity, and provides the desired electrochemical functions; the support matrix may provide mechanical support, and it may also serve to 15 protect the solid acid from water in the environment. A high temperature of operation can render the solid acid into its superprotomic state. A high temperature of operation can also ensure that any water present in the electrochemical device will be present in the form of steam rather than liquid water, making 20 the H₂O less likely to attack the solid acid.

Hydrogen/Air Fuel Cells

A hydrogen/air fuel cell is shown in Figure 1, in which the proton conducting membrane is a solid acid/matrix composite of the type described herein. Because the membrane need not be humidified, the fuel cell system can be simpler than one which uses a hydrated polymer membrane. The humidification system normally required for fuel cell utilizing a Nafion or related polymer membrane can be eliminated in Figure 1. Hence, less rigid temperature monitoring and control may be used in the solid acid based system as compared with Nafion based fuel cell systems. These differences allow a less-costly fuel cell system.

Because the membrane need not be humidified, the fuel cell shown in Fig. 1 can be operated at temperatures above 100°C. The tolerance of the Pt/Ru catalysts to carbon monoxide CO poisoning increases with increasing temperature. Thus, a fuel cell such as shown in Fig. 1, operated at a temperature above 100°C may withstand higher concentrations of CO in the hydrogen fuel than a Nafion based fuel cell which is typically operated at a temperature lower than 100°C.

The high temperature of operation also enhances the kinetics of the electrochemical reactions, and can thereby result in a fuel cell with higher overall efficiency than one based on Nafion or other hydrated polymers.

5

Direct Methanol Fuel Cells

A direct methanol fuel cell is shown in Figure 2. The proton conducting membrane is a solid acid/matrix composite of the type described herein. Because the membrane need not be humidified, the fuel cell system is much simpler and thus less costly than state of the art direct methanol fuel cell systems. The humidification system normally required for fuel cell utilizing a Nafion or related polymer membrane is eliminated in Figure 2. Furthermore, temperature monitoring and control in the solid acid based system does not need to be as tight as in Nafion based fuel cell systems. Because the solid acid based membrane need not be humidified, the fuel cell may be operated at elevated temperatures. High temperatures can enhance the kinetics of the electrochemical reactions. This can result in a fuel cell with very high efficiency.

Another significant advantage of the fuel cell shown in Figure 2 over state of the art direct methanol fuel cells results from the decreased permeability of the membrane to methanol. In state of the art direct methanol fuel cells, in which Nafion or another hydrated polymer serves as the membrane, methanol cross-over through the polymeric membrane lowers fuel cell efficiencies. The impermeability of a solid acid membrane can improve this efficiency.

10 **Hydrogen Separation Membranes**

The Ru/Pt catalyst in a hydrogen/air fuel cell is sensitive to CO poisoning, particularly at temperatures close to ambient. Therefore, in an indirect hydrogen/air fuel cell, the hydrogen produced by the reformer is often cleaned, of e.g. CO to below 15 50ppm, before it enters the fuel cell for electrochemical reaction.

In Figure 3, a hydrogen separation membrane is shown for the removal of CO and other gases from hydrogen. The hydrogen separation membrane is made of a mixed proton and electron 20 conducting membrane, as described herein. Hydrogen gas, mixed with other undesirable gases, is introduced onto one side of the membrane. Clean hydrogen gas is extracted from the other side of the membrane.

On the inlet side of the membrane, hydrogen gas is dissociated into H⁺ and e⁻. Because the membrane is both proton conducting and electron conducting, both of these species can migrate through the membrane. However, the membrane is substantially impermeable to other gases and fluids. Hence, CO and other undesirable gases or fluids cannot so migrate. On the outlet side of the membrane, the H⁺ and e⁻ recombine to form hydrogen gas. The overall process is driven by the hydrogen chemical potential gradient, which is high on the inlet side of the membrane and low on the outlet side of the membrane.

Another type of hydrogen separation membrane is shown in Figure 4. The membrane is made of a proton conducting composite of the type described herein, and is connected to a current source. Hydrogen gas, mixed with other undesirable gases, is introduced onto one side of the membrane and clean hydrogen gas is extracted from the other side of the membrane. Application of a current causes the hydrogen gas to dissociate into H⁺ and e⁻. Because the membrane conducts only protons, these protons are the only species which can migrate through the membrane. The electrons migrate through the current source to the outlet side of the membrane, where the H⁺ and e⁻ recombine to form hydrogen gas. The membrane is substantially impervious to other gases and fluids. Hence, CO and other undesirable gases or fluids cannot migrate through the proton conducting membrane. The overall process is driven by electric current applied via the current source.

Membrane Reactors

In Figure 5 a membrane reactor is shown, in which a mixed proton and electron conducting membrane of the type described herein is utilized. The general reaction is that reactants A + B react to form products C + D, where D is hydrogen gas. Use of a 5 mixed proton and electron conducting membrane in this reactor can enhance the reaction to give yields that exceed thermodynamic equilibrium values. On the inlet side of the membrane reactor, the reactants form products C + H₂. Under equilibrium conditions, the hydrogen concentration builds up and the forward 10 reaction is slowed. With the use of the mixed hydrogen and electron conducting membrane, the hydrogen is immediately extracted from the reaction region via transport through the membrane, and the forward reaction is enhanced. Examples of reactions in which yield could be enhanced by using such a 15 membrane reactor include (1) the steam reformation of methane (natural gas) to produce syngas: CH₄ + H₂O → CO + 3H₂; (2) the steam reformation of CO to produce CO₂ and H₂: CO + H₂O → CO₂ + H₂; (3) the decomposition of H₂S to H₂ and S, (4) the decomposition of NH₃ to H₂ and N₂; (4) the dehydrogenation of 20 propane to polypropylene; and (5) the dehydrogenation of alkanes and aromatic compounds to various products.

In Figure 6 a second type of membrane reaction is shown, again, utilizing a mixed proton and electron conducting membrane of the type described herein. In this case, the general reaction is that the reactants A + B form the products C + D, where B is 5 hydrogen. The hydrogen enters the reaction region via transport through the mixed conducting membrane, whereas the reactant A is introduced at the inlet to the membrane reactor, and is mixed with other species. The manner in which the hydrogen is introduced into the reactant stream (through the membrane) 10 ensures that only the reactant A, and none of the other species reacts with hydrogen. This effect is termed selective hydrogenation.

The mixed proton and electron conducting membranes described herein provide an advantage over state-of-the-art membranes in 15 that the conductivity is high at temperatures as low as 100°C, and the membranes are relatively inexpensive. Selective hydrogenation at temperatures close to ambient may have particular application in synthesis of pharmaceutically important compounds which cannot withstand high temperatures.

According to a first class of materials, the solid acid is mixed with a supporting structure that is electrochemically unreactive, to form a composite. A first embodiment uses a solid acid mixed with a melt-processable polymer as the supporting 5 matrix structure.

The solid acid (CHS) was prepared from aqueous solutions containing stoichiometric amounts of Cs₂CO₃ and H₂SO₄. Crystalline CsHSO₄ and a small amount (~ 8 wt%) of the related compound Cs₅H₃(SO₄)₄•xH₂O (which also exhibits superprotic 10 behavior) were obtained upon introduction of methanol into the solution. Composite membranes of the solid acid and poly(vinylidene fluoride) were prepared by simple melt-processing methods. The two components were lightly ground together then hot-pressed at 180 °C and 10 kpsi for 15 minutes. Volume ratios 15 of CHS:PVDF from 100% CsHSO₄ to 100% PVDF were prepared in 10 vol% increments.

Another example of a composite contains a solid acid and a thermoset polymer, which can be mixed in with the solid acid in monomer or prepolymer form, and then polymerized in situ.

The solid acid (CHS) was prepared from aqueous solutions containing stoichiometric amounts of Cs_2CO_3 and H_2SO_4 . Crystalline CsHSO_4 and a small amount (~ 8 wt%) of the related compound $\text{Cs}_5\text{H}_3(\text{SO}_4)_4 \bullet x\text{H}_2\text{O}$ (which also exhibits superprotonic behavior) were obtained upon introduction of methanol into the solution. Composite membranes of the solid acid and the polyester resin marketed under the name Castoglas by Buehler, Inc. were synthesized simply by lightly grinding the solid acid and pre-polymer together and then adding the polymerization/crosslinking catalyst. A material with a 50:50 volume ratio was prepared.

Another example of a thermoset polymer - solid acid composite comprises the solid acid $(\text{NH}_3)_3\text{H}(\text{SO}_4)_2$ and the polymer poly(dicyclopentadiene) or poly DCPD.

The solid acid, TAHS, was prepared from aqueous solutions of $(\text{NH}_4)_2\text{SO}_4$ and H_2SO_4 . The solid acid was ground then mixed with the monomer dicyclopentadiene. The polymerization catalyst was introduced into the mixture, which was then poured onto a Teflon plate and pressed into a thin film. The film was cured at 100°C for approximately 2 hours. Materials with 25 and 17 vol % TAHS were prepared.

Another method for preparing solid acid/polymer composites is suspension coating. For this, CsHSO₄ was dissolved in a water/ethanol solution. The polymer PVDF was then dispersed into this solution. A composite membrane was formed by casting the 5 suspension and allowing the solvents to evaporate. Composite membranes comprised of a solid acid and a non-polymeric matrix material, such as a ceramic or an oxide glass can be prepared in the following manner. The solid acid is synthesized from aqueous solution and the matrix material is synthesized separately. The 10 two components are mixed and ground together. The mixture is then hot pressed, preferably at a temperature which causes the solid acid to melt and flow, to yield a dense composite membrane.

The nature of the chemical bonding in solid acids of general formula M_aH_b(XO₄)_c·nH₂O or M_aH_b(XO₃)_c·nH₂O where:

15 M is one or more of the species in the group consisting of Li, Be, Na, Mg, K, Ca, Rb, Sr, Cs, Ba, Tl and NH₄⁺;

X is one or more of the species in the group consisting of Si, P, S, As, Se, and Te; and

a, b, c, and n are rational numbers, and n can be zero.

20 leads to materials which are inherently poor conductors of electrons. These compounds can be used in devices which require both proton and electron transport directly through the membrane if a mechanism for electron transport is introduced.

The first approach for introducing electronic conductivity into solid acid based materials is to prepare a composite comprised of the solid acid and a second substance which has a high electronic conductivity. This second substance may be an 5 electronically conducting polymer, such as poly(aniline), or a typical metal, such as aluminum or copper. Where the electronically conducting component is a metal, it may be advantageous to introduce a chemically and electrically inert polymer into the composite simply to serve as a binder and 10 provide the membrane with good mechanical properties. The processing methods described above may be used to prepare such composite membranes.

The second approach for introducing electronic conductivity into solid acid based materials is to perform direct chemical substitutions with variable valence ions. For example, a portion of the sulfur in CsHSO₄ may be replaced by chromium, which can be 5 present in an oxidation state of anywhere from 2+ to 6+. Similarly, manganese may be introduced on the sulfur site, as this ion exhibits valence states anywhere between 2+ and 7+. Chemical substitution may also be performed with respect to the cesium in a compound such as CsHSO₄. Large ions with variable 10 valence, such as thallium, indium, lead and tin can be used for these substitutions. The solid acid so modified may be used in an electrochemical device directly, or may be combined with a supporting matrix material as described above.

In the Figure 1 embodiment, a membrane-electrode assembly (MEA) is prepared from the CHS-PVDF composite film in which the solid acid to polymer volume ratio is 50:50. The electrodes are formed of graphite paper which is impregnated with a complex slurry of platinum powder, PVDF, the solid acid, and Nafion, suspended/dissolved in a water and isopropanol solution. After evaporation of the solvents, the electrodes so prepared are hot-pressed onto the composite membrane. The MEA is placed in a fuel cell test station at 140°C and hydrogen is introduced at the anode and oxygen at the cathode. The open cell voltage (OCV) obtained in this manner was 0.88 V. The same type of MEA may also be used in the Fig 2 embodiment.

VII. Examples

Example 1

A Cs based solid acid such as CsHSO₄, CsHSeO₄ or Cs₅H₃(SO₄)₄·xH₂O is ground and mixed with a melt-processable polymer binder, such as poly(vinylidene fluoride), and hot-pressed. The result forms a solid composite membrane which is proton conducting even in dry atmospheres. The composite membrane, being comprised of two components which are substantially impermeable to fluids,, may be less permeable than Nafion™.

Example 2

A Cs based solid acid such as $\text{Cs}_3(\text{HSO}_4)_2(\text{H}_{1.5}(\text{S}_{0.5}\text{P}_{0.5})\text{O}_4)$, $\text{Cs}_3(\text{HSO}_4)_2(\text{H}_2\text{PO}_4)$, $\text{Cs}_5(\text{HSO}_4)_3(\text{H}_2\text{PO}_4)_2$ or $\text{Cs}_2(\text{HSO}_4)(\text{H}_2\text{PO}_4)$ is ground
5 and mixed with a melt-processable polymer binder, such as poly(vinylidene fluoride), and hot-pressed. The result forms a solid composite membrane which is proton conducting even in dry atmospheres. The membrane is also less permeable to fluids than NafionTM.

10

Example 3.

A NH₄ based solid acid such as $(\text{NH}_4)_3\text{H}(\text{SO}_4)_2$ or $(\text{NH}_4)_3\text{H}(\text{SeO}_4)_2$ is ground and mixed with a melt-processable polymer binder, such as Crystar 101 thermoplastic, and hot-pressed. The result forms
15 a solid composite membrane which is proton conducting even in dry atmospheres. The membrane is less permeable to fluids than NafionTM and is also less expensive.

Example 4.

An solid acid silicate of general formula $M_aH_bSiO_4$, such as $CaNaHSiO_4$, Cs_3HSiO_4 , $(NH_4)_3HSiO_4$, is used as a membrane. Some of these materials are water insoluble and may have sufficient structural integrity that a binder is not required in some 5 applications.

Example 5.

A Cs or NH₄ based solid acid, such as CsHSO₄, Cs₂(HSO₄)(H₂PO₄), Cs₅H₃(SO₄)₄ • x H₂O or (NH₄)₃H(SO₄)₂ is mixed with 10 the prepolymer of a resin such as "castoglas", a commercial product from Buehler, Inc. The polymerization/crosslinking catalyst is added to the mixture, and a solid composite membrane so formed. The in situ polymerization/crosslinking can lead to a higher impermeability than composites formed by melt-processing.

15

Example 6.

A Cs or NH₄ based solid acid, such as CsHSO₄, Cs₂(HSO₄)(H₂PO₄), Cs₅H₃(SO₄)₄ •xH₂O or (NH₄)₃H(SO₄)₂ is mixed with a monomer such as dicyclopentadiene. A polymerization catalyst is then added to the mixture, and a solid composite membrane
5 comprised of the solid acid and poly(dicyclopentadiene) is formed. The in situ polymerization of the polymer can lead to a higher impermeability than composites formed by melt-processing.

Use of a NH₄ based solid acid can result in an inexpensive membrane.
10 Example 7.

A Cs or NH₄ based solid acid, such as CsHSO₄, Cs₂(HSO₄)(H₂PO₄), Cs₅H₃(SO₄)₄ xH₂O or (NH₄)₃H(SO₄)₂ is dissolved in water, and added to a suspension of an insoluble polymer such as poly(vinylidene fluoride) suspended in a fluid such as ethanol.
15 The mixture is cast and the liquids (water and ethanol) allowed to evaporate. This procedure yields a composite membrane which is proton conducting even in dry atmospheres. The casting step can produce very thin membranes, with thicknesses on the order of one hundred microns.

Example 8.

A Cs or NH₄ based solid acid, such as CsHSO₄,
Cs₂(HSO₄) (H₂PO₄), Cs₅H₃(SO₄)₄ •xH₂O or (NH₄)₃H(SO₄)₂ is ground and
5 mixed with a ceramic, such as Al₂O₃, or an oxide glass, such as
amorphous SiO₂. The mixed powders are compressed by hot-
pressing. The resulting composite membrane may be stable to
higher temperatures than those in which the binder is a polymer.

10 Example 9.

A Cs or NH₄ based solid acid, such as CsHSO₄,
Cs₂(HSO₄) (H₂PO₄), Cs₅H₃(SO₄)₄ •xH₂O or (NH₄)₃H(SO₄)₂ is dissolved in
water. The solution is introduced into a porous membrane
comprised of an inert binder such as TeflonTM, SiO₂, or Al₂O₃.
15 The water is allowed to evaporate, leaving the solid acid to fill
the pores of the binder. The result is a composite membrane
which is proton conducting even in dry atmospheres.

Example 10.

A Cs or NH₄ based solid acid, such as CsHSO₄, Cs₂(HSO₄)(H₂PO₄), Cs₅H₃(SO₄)₄ •xH₂O or (NH₄)₃H(SO₄)₂, which is only proton conducting, is ground and mixed with an electronically conducting polymer such as poly(anylene). The composite membrane
5 formed can conduct both protons and electrons.

Example 11.

An solid acid silicate of general formula M_aH_bSiO₄, such as CaNaHSiO₄, Cs₃HSiO₄ or (NH₄)₃HSiO₄, is ground and mixed with an
10 electronically conducting polymer such as poly(anilene). The composite membrane formed can conduct both protons and electrons.

Example 12.

A proton conducting solid acid, such as CsHSO₄,
15 Cs₂(HSO₄)(H₂PO₄), (NH₄)₃H(SO₄)₂ or CaNaHSiO₄, and a metal, such as Ag, Au, or Cu, are ground and mixed. The mixed powders are compressed by hot-pressing. The composite membrane formed can conduct both protons and electrons, and may be stable to higher temperatures than a composite in which the electron conducting
20 component is a polymer.

Example 13.

A proton conducting solid acid, such as CsHSO_4 , $\text{Cs}_2(\text{HSO}_4)(\text{H}_2\text{PO}_4)$, $(\text{NH}_4)_3\text{H}(\text{SO}_4)_2$ or CaNaHSiO_4 , and a metal, such as Ag, Au, or Cu, are ground and mixed. A polymeric material is also added. A solid composite membrane is prepared either by 5 hot-pressing, if the polymer is melt-processable such as poly(vinylidene fluoride), or by in situ polymerization, if the polymer is in situ polymerizable such as poly(dicyclopentadiene). The composite membrane is both proton and electron conducting, and may have superior mechanical properties to a composite 10 containing only a solid acid and a metal.

Example 14.

A mixed electron and proton conducting solid acid, such as $\text{CsHCr}_x\text{S}_{1-x}\text{O}_4$ or $(\text{NH}_4)_3\text{H}(\text{Cr}_x\text{S}_{1-x}\text{O}_4)_2$ in which one of the X elements 15 has a variable valence, is mixed with an inert polymeric binder. If the polymer is melt-processable, such as poly(vinylidene fluoride), a membrane is formed by hot-pressing. If the polymer can be polymerized in situ, a membrane is formed by mixing the solid acid, the monomer and the polymerization catalyst. The 20 resulting membrane conducts both protons and electrons, and may be more stable in oxidizing atmospheres than a composite containing metal particles.

Example 15.

A Cs or NH₄ based solid acid, such as CsHSO₄,

Cs₂(HSO₄)(H₂PO₄), Cs₅H₃(SO₄)₄ •xH₂O or (NH₄)₃H(SO₄)₂ is prepared from
5 aqueous solution, ground, and then pressed into a thin membrane.

The membrane is used in an electrochemical device at a temperature above the superprotic transition temperature and above 100°C, so that the proton conductivity of the solid acid is high and any H₂O that may be present in the device exists in the
10 form of steam rather than liquid water.

Example 16.

A mixed electron and proton conducting solid acid, such as CsHCr_xS_{1-x}O₄ or (NH₄)₃H(Cr_xS_{1-x}O₄)₂ in which one of the X elements
15 has a variable valence, is prepared from aqueous solution or by solid state reaction. The powder is then ground and pressed into a thin membrane. The membrane is used in an electrochemical device at a temperature above the superprotic transition temperature and above 100°C, so that the conductivity of the
20 solid acid is high and any H₂O that may be present in the device exists in the form of steam rather than liquid water.

Example 17.

A composite comprised of one or more of the solid acids listed in Table 1 and one or more of inert binders listed in Table 2. If one or more of the components in the composite is electronically conducting, the composite membrane will be capable 5 of conducting both protons and electrons. Electronically conducting substances are indicated.

Table 1. Solid acid compounds.

Sulfates and sulfate-phosphates	selenates and selenate phosphates	silicates
CsHSO ₄	CsHSeO ₄	CaNaHSiO ₄
Cs ₃ H(SO ₄) ₂	Cs ₃ H(SeO ₄) ₂	CaH ₂ SiO ₄
Cs ₅ H ₃ (SO ₄) ₄ · xH ₂ O	Cs ₅ H ₃ (SeO ₄) ₄ · xH ₂ O	CsH ₃ SiO ₄
Cs ₃ (HSO ₄) ₂ (H _{1.5} (S _{0.5} P _{0.5})O ₄)	Cs ₃ (HSeO ₄) ₂ (H _{1.5} (Se _{0.5} P _{0.5})O ₄)	Cs ₂ H ₂ SiO ₄
Cs ₃ (HSO ₄) ₂ (H ₂ PO ₄)	Cs ₃ (HSeO ₄) ₂ (H ₂ PO ₄)	Cs ₃ HSiO ₄
Cs ₂ (HSO ₄) ₂ (H ₂ PO ₄)	Cs ₂ (HSeO ₄) ₂ (H ₂ PO ₄)	NH ₄ H ₃ SiO ₄
Cs ₅ (HSO ₄) ₃ (H ₂ PO ₄) ₂	Cs ₅ (HSeO ₄) ₃ (H ₂ PO ₄) ₂	(NH ₄) ₂ H ₂ SiO ₄
CsH ₂ PO ₄		(NH ₄) ₃ HSiO ₄
NH ₄ HSO ₄	NH ₄ HSeO ₄	RbH ₃ SiO ₄
(NH ₄) ₃ H(SO ₄) ₂	(NH ₄) ₃ H(SeO ₄) ₂	Rb ₂ H ₂ SiO ₄
(NH ₄) ₅ H ₃ (SO ₄) ₄ · xH ₂ O	(NH ₄) ₅ H ₃ (SeO ₄) ₄ · xH ₂ O	Rb ₃ HSiO ₄
(NH ₄) ₂ (HSO ₄) ₂ (H ₂ PO ₄)	(NH ₄) ₂ (HSeO ₄) ₂ (H ₂ PO ₄)	KH ₃ SiO ₄

$(\text{NH}_4)_2\text{H}_2\text{PO}_4$		$\text{K}_2\text{H}_2\text{SiO}_4$
RbHSO_4	RbHSeO_4	K_3HSiO_4
$\text{Rb}_3\text{H}(\text{SO}_4)_2$	$\text{Rb}_3\text{H}(\text{SeO}_4)_2$	NaH_3SiO_4
$\text{Rb}_5\text{H}_3(\text{SO}_4)_4 \cdot x\text{H}_2\text{O}$	$\text{Rb}_5\text{H}_3(\text{SeO}_4)_4 \cdot x\text{H}_2\text{O}$	$\text{Na}_2\text{H}_2\text{SiO}_4$
$\text{Rb}_2(\text{HSO}_4)(\text{H}_2\text{PO}_4)$	$\text{Rb}_2(\text{HSeO}_4)(\text{H}_2\text{PO}_4)$	Na_3HSiO_4
RbH_2PO_4		BaCsHSiO_4

Table 2. Binder or matrix materials

Polymer	ceramic/oxide glass	metal or semiconductor
poly(vinylidene fluoride)	SiO_2	Ag*
poly(dicyclopentadiene)	Al_2O_3	Au*
poly(tetraflouoroethelyne) [Teflon]	MgO	Cu*
poly(ether-ether ketone)	cordierite	Al*
poly(ether sulfone)		Ni*
Silicones [dimethyl siloxane polymers]		Fe*
poly(pyrrole)*		Zn*
poly(aniline)*		graphite*
		silicon*

* electronically conducting

Other modifications are within the disclosed embodiment. For example, the above has described the materials having a superprot tonic transition upon heating. Certain materials may have their superprot tonic transition temperature below room 5 temperature. Thus, there may be no apparent superprot tonic transition and the material would be disordered at room temperature. These solid acids with structural disorder even prior to heating are also contemplated.

10

What is claimed is:

1. A proton conducting membrane, formed of a solid acid
5 material in a solid phase.

2. A membrane as in claim 1 wherein said solid acid
material is of a type that is capable of a superprotomeric
transition.

10

3. A membrane as in claim 1 wherein said solid acid
material is of the general form $M_aH_b(XO_t)_c$

4. A membrane as in claim 3 wherein t is 3 or 4.

15

5. A membrane as in claim 1 wherein said solid acid
material is of the general form $Cs_aH_b(XO_t)_c$.

6. A membrane as in claim 3 where X is silicon.

20

7. A membrane as in claim 4 wherein M is Cs.

25

8. A membrane as in claim 4 wherein M is NH_4 .

9. A membrane as in claim 4 wherein said solid acid is of the form $M_aH_b(XO_t)_c \cdot nH_2O$.

10. A membrane as in claim 4 wherein X is P.
5

11. A membrane as in claim 3, wherein said solid acid is CsH_2PO_4 .

10

12. A membrane as in claim 3, wherein said solid acid is $Cs_5(HSO_4)_3(H_2PO_4)_2$.

15

13. A membrane as in claim 3, wherein said solid acid is $Cs_2(HSO_4)_x(H_2PO_4)_y$.

20

14. A membrane as in claim 3, wherein said solid acid is $Cs_3(HSO_4)_2(H_{1.5}(S_{0.5}P_{0.5})O_4)$.

25

15. A membrane as in claim 3, wherein said solid acid is $Cs_5H_3(SO_4)_4 \cdot xH_2O$.

30

16. A membrane as in claim 3, wherein said solid acid is $TlHSO_4$.

17. A membrane as in claim 3, wherein said solid acid is
CsH(SeO₄)_x.

5

18. A membrane as in claim 3, wherein said solid acid is
Cs₂(HSeO₄) (H₂PO₄) .

19. A membrane as in claim 3, wherein said solid acid is
10 (NH₄)₃H(SO₄)₂.

20. A membrane as in claim 3, wherein said solid acid is
(NH₄)₂(HSO₄) (H₂PO₄) .

15

21. A membrane as in claim 3, wherein said solid acid is
Rb₃H(SO₄)₂.

20

22. A membrane as in claim 3, wherein said solid acid is
Rb₃H(SeO₄)₂.

25

23. A membrane as in claim 3, wherein said solid acid is
Cs_{1.5}Li_{1.5}H(SO₄)₂.

30

24. A membrane as in claim 3, wherein said solid acid is
 $\text{Cs}_2\text{Na}(\text{HSO}_4)_3$.

5

25. A membrane as in claim 3, wherein said solid acid is
 $\text{TlH}_3(\text{SeO}_3)_2$.

10

26. A membrane as in claim 3, wherein said solid acid is
 CsH_2AsO_4 .

15

27. A membrane as in claim 3, wherein said solid acid is
 $(\text{NH}_4)_2(\text{HSO}_4)(\text{H}_2\text{AsO}_4)$.

20

28. A membrane as in claim 3, wherein said solid acid is
 CaNaHSiO_4 .

25

29. A membrane as in claim 3, further comprising an
electrochemical device, using said membrane for proton transport.

30. A membrane as in claim 1 wherein said solid acid
material is formed of a material that is not water soluble.

31. A proton conducting membrane, formed of an solid acid material in a superprotic phase, said solid acid material being
5 of the general formula $M_aH_b(XO_t)_c$, where t is 3 or 4;
the M material is at least one material from the group consisting of Li, Be, Na, Mg, K, Ca, Rb, Sr, Cs, Ba, Tl or NH_4^+ , and the X material is at least one material from the group consisting of Si, P, S, As, Se, or Te.

10

32. A membrane as in claim 31 wherein said solid acid is non-water soluble.

33. A method of conducting protons across a barrier,
comprising:

5 forming a membrane from a solid acid material; and
using said solid acid material to conduct protons.

34. A method as in claim 33, wherein said solid acid is of
a type that is capable of a superprotic transition between a
first temperature and a second temperature; and
10 operating said membrane as a proton conducting membrane at a
temperature between said first and second temperatures.

35. A method as in claim 33 wherein said solid acid
material is of the general form $M_aH_b(XO_t)_c$.

15

36. A method as in claim 35 wherein M is Cs.

37. A method as in claim 35 wherein M is NH_4^+ .

20 38. A method as in claim 35 wherein X includes silicon.

39. A method as in claim 33 wherein said protons are
conducted in a fuel cell.

40. A method as in claim 33 wherein said protons are conducted in a hydrogen separator.

5 41. A method as in claim 33 wherein said protons are conducted in an electrolysis cell.

42. A method as in claim 33 wherein said protons are conducted in a battery.

10

43. A proton conducting membrane, comprising:
an solid acid material; and
a structural binder for said solid acid material, forming a membrane with said solid acid material.

15

44. A membrane as in claim 43 wherein said structural binder is a polymer.

20 45. A membrane as in claim 44 wherein said solid acid material is a type capable of a superprotomic transition at a specified temperature.

46. A membrane as in claim 43 wherein said solid acid

material is a non-water soluble solid acid material.

47. A membrane as in claim 44 wherein said polymer is a melt processable polymer.

5

49. A membrane as in claim 44 wherein said polymer is an in-situ polymerized polymer.

50. A membrane as in claim 43 wherein said structural
10 binder is a ceramic.

51. A membrane as in claim 43 wherein said structural binder is a glass.

15 52. A membrane as in claim 43 wherein said structural binder is electronically insulating.

53. A membrane as in claim 43 wherein said structural binder is electrically conducting.

20

54. A membrane as in claim 53 wherein said conducting material is a conducting polymer.

55. A membrane as in claim 53 wherein said conducting material is a metal.

56. A membrane as in claim 55 wherein said metal is mixed 5 with a polymer.

57. A membrane as in claim 53 wherein said conductor is formed by direct chemical substitution with variable valence ions.

10

58. A membrane as in claim 43 wherein said structural binder includes silicon.

59. A membrane as in claim 43 wherein said structural 15 binder is a polyester binder.

60. A membrane as in claim 43 wherein said structural binder is electrochemically unreactive.

20 61. A membrane as in claim 43 wherein said solid acid is of the of the general formula $M_aH_b(XO_t)_c$, where:

the M material is a material from the group consisting of Li, Be, Na, Mg, K, Ca, Rb, Sr, Cs, Ba, Te or NH₄⁺, and

the X material is from the group consisting of Si, P, S, As, Se, or Te.

5

62. A membrane as in claim 61 wherein M is Cs.

63. A membrane as in claim 61 wherein X is Si.

10

64. A membrane as in claim 61 where M is NH₄⁺.

65. A membrane as in claim 61 wherein said solid acid material is a solid acid material.

15

66. A membrane as in claim 61 wherein said solid acid material is water insoluble.

67. A membrane as in claim 53 wherein said solid acid material is processed to include variable valence elements.

20

67. A fuel cell comprising:

a source of fuel; and

a proton conducting membrane, formed of an solid acid material in a superprotic phase.

68. A fuel cell as in claim 67, wherein said solid acid
5 material is water insoluble.

69. A fuel cell as in claim 67, wherein said solid acid material is of the general formula $M_aH_b(XO_t)_c$, where:

the M group is a material from the group consisting of
10 Li, Be, Na, Mg, K, Ca, Rb, Sr, Cs, Ba, Tl or NH_4^+ , and
the X material is from the group consisting of Si, P,
S, As, Se, or Te.

70. A method of operating an electrochemical device
15 comprising:

providing a fuel to a proton conducting membrane;
and
carrying out an electrochemical reaction at said proton
conducting membrane, without humidifying said membrane.

20
71. A method as in claim 70, wherein said carrying out
comprises operating at a temperature of 100° degrees C or higher.

72. A method as in claim 70, wherein said proton conducting membrane includes an solid acid material.

5 73. A method as in claim 70, wherein said proton conducting membrane includes an solid acid material in a superprotontic phase.

10 74. A method as in claim 72, wherein said proton conducting membrane includes a binder.

75. A method as in claim 74, wherein said solid acid material is of the general formula $M_aH_b(XO_4)_c$, where:

the M group is a material from the group consisting of
5 Li, Be, Na, Mg, K, Ca, Rb, Sr, Cs, Ba, Tl or NH_4^+ , and
the X material is from the group consisting of Si, P,
S, As, Se, or Te.

76. A proton and electron conducting membrane, formed of an
10 solid acid material.

77. A membrane as in claim 76 wherein said solid acid material is of a type that is capable of a superprot tonic transition at a specified temperature.

15

78. A membrane as in claim 76 wherein said solid acid material is of the general formula $M_aH_b(XO_t)_c$.

79. A membrane as in claim 76 wherein said solid acid
20 material is a solid acid material.

80. A membrane as in claim 78 where X includes silicon.

81. A membrane as in claim 76, further comprising a binder for the solid acid material.

82. A membrane as in claim 76 wherein said binder includes
5 a conducting material.

83. A membrane as in claim 82 wherein said conducting material includes a conductive polymer.

10 84. A membrane as in claim 82 wherein said conducting material includes a metal material.

85. A membrane as in claim 76 wherein said solid acid material has free valence electrons.

15

86. A method of separating H₂ from other materials, comprising:

chemically reacting a H₂ at a surface of a proton and electron conducting membrane which is formed of materials
20 including a solid acid material, to decompose said H into H⁺ and e⁻; and

using said membrane formed of an solid acid material to allow said H⁺ and e⁻ to pass while blocking other materials including CO from passing.

5 87. A proton conducting membrane comprising;
a Cs based solid acid material; and
a melt processable polymer binder for said solid acid material, forming a membrane with said solid acid material.

10 88. A membrane as in claim 87 wherein said Cs based solid acid is one of Cs₃(HSO₄)₂(H_{1.5}(S_{0.5}P_{0.5})O₄) , Cs₃(HSO₄)₂(H₂PO₄) , Cs₅(HSO₄)₃(H₂PO₄)₂ or Cs₂(HSO₄)(H₂PO₄) CsHSO₄, CsHSeO₄ or Cs₅H₃(SO₄)₄·xH₂O.

15 89. A membrane as in claim 87 wherein said melt processable polymer is polyvinylidene fluoride.

90. A membrane as in claim 87 wherein said membrane is formed by hot pressing.

20 91. A proton conducting membrane, comprising:
a NH₄ based solid acid material; and

a structural binder for said solid acid material, forming a membrane with said solid acid material.

92. A membrane as in claim 91 wherein said structural
5 binder is a melt processable polymer.

93. A membrane as in claim 91 wherein said solid acid is one of CsH_2PO_4 , $\text{Cs}_5(\text{HSO}_4)_3(\text{H}_2\text{PO}_4)_2$, $\text{Cs}_2(\text{HSO}_4)(\text{H}_2\text{PO}_4)$,
 $\text{Cs}_3(\text{HSO}_4)_2(\text{H}_2\text{PO}_4)$, $\text{Cs}_3(\text{HSO}_4)_2(\text{H}_{1.5}(\text{S}_{0.5}\text{P}_{0.5})\text{O}_4)$, $\text{Cs}_5\text{H}_3(\text{SO}_4)_4 \cdot x\text{H}_2\text{O}$,
10 TlHSO_4 , CsHSeO_4 , $\text{Cs}_2(\text{HSeO}_4)(\text{H}_2\text{PO}_4)$, $\text{Cs}_3\text{H}(\text{SeO}_4)_2 (\text{NH}_4)_3\text{H}(\text{SO}_4)_2$,
 $(\text{NH}_4)_2(\text{HSO}_4)(\text{H}_2\text{PO}_4)$, $\text{Rb}_3\text{H}(\text{SO}_4)_2$, $\text{Rb}_3\text{H}(\text{SeO}_4)_2$, $\text{Cs}_{1.5}\text{Li}_{1.5}\text{H}(\text{SO}_4)_2$,
 $\text{Cs}_2\text{Na}(\text{HSO}_4)_3$, $\text{TlH}_3(\text{SeO}_3)_2$, $\text{CsH}_2\text{AsO}_4 (\text{NH}_4)_2(\text{HSO}_4)(\text{H}_2\text{AsO}_4)$, TeO_4 , or
 CaNaHSiO_4 .

15 94. A proton conducting membrane, comprising:
a solid acid silicate of the general form $\text{M}_\text{A}\text{H}_\text{B}\text{SiO}_4$ used in a
proton conducting membrane.

95. A membrane as in claim 94 further comprising a
20 structural binder for said solid acid material.

96. A membrane as in claim 94 wherein said solid acid is one of CaNaHSiO_4 , Cs_3HSiO_4 or $(\text{NH}_4)_3\text{HSiO}_4$.

97. A proton conducting membrane, comprising:
a Cs or NH₄ based solid acid; and
a ceramic or glass binder, forming a structural binder for
5 said solid acid.

98. A device as in claim 97 wherein said binder is porous.

99. A method of using an electrochemical device,
10 comprising:
forming a solid acid material into a proton conducting
membrane; and
using said solid acid membrane to conduct protons.
15 100. A method as in claim 99 further comprising heating said
solid solid acid material to a temperature at which it undergoes
a superprotic transition, prior to said using.

101. A method as in claim 99 wherein said solid solid acid
20 compound is a sulfate or sulfate phosphate type solid acid.

102. A method as in claim 99 wherein said solid solid acid
compound is a selenate or selenate phosphate solid acid.

103. A method as in claim 99 wherein said solid solid acid
is a silicate.

5 104. A method as in claim 99 wherein said forming comprises
adding a binder to said material.

105. A method as in claim 104 wherein said binder is a
polymer.

10

106. A method as in claim 104 wherein said binder is a
ceramic/oxide glass.

107. A material as in claim 104 wherein said binder is a
15 conducting metal or semiconductor.

108. A method of operating an electrochemical device,
comprising:

20 forming a membrane using a solid acid material of the
general form $M_aH_b(XO_t)_c$; and
using said solid solid acid material to conduct protons in
the electrochemical device.

109. A membrane as in claim 31, wherein said solid acid is a solid solid acid material.

110. A proton conducting membrane, formed of a solid acid 5 material in a superprotic phase.

111. A method of operating an electrochemical device comprising:

providing a fuel to a proton conducting membrane which 10 includes a carbon monoxide material therein,

and

carrying out an electrochemical reaction at said proton conducting membrane, without removing said carbon monoxide 20 material.

15

112. A method of forming a membrane-electrode assembly, comprising:

forming a composite film including a polymer and a solid acid of the general form $M_aH_b(XO_t)_c$;

20 forming said composite film onto a backing;

forming electrodes on said backing; and

hot pressing said material to form an assembly.

113. A method as in claim 112, wherein an solid acid to polymer volume ratio is 50/50.

5 114. A method as in claim 112, wherein said backing is graphite paper.

115. A method as in claim 33, wherein said protons are conducted in a supercapacitor.

1/2

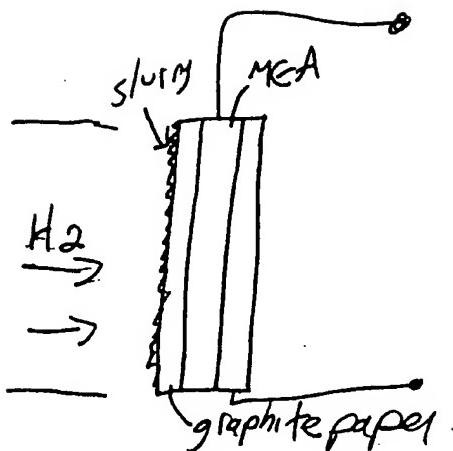


FIG 1

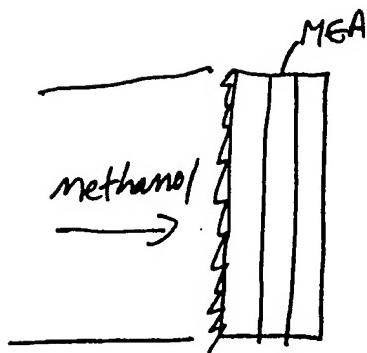


FIG 2

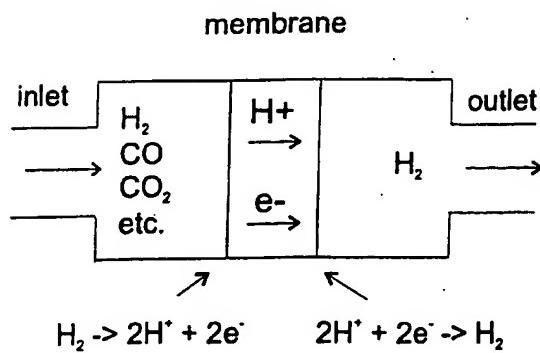
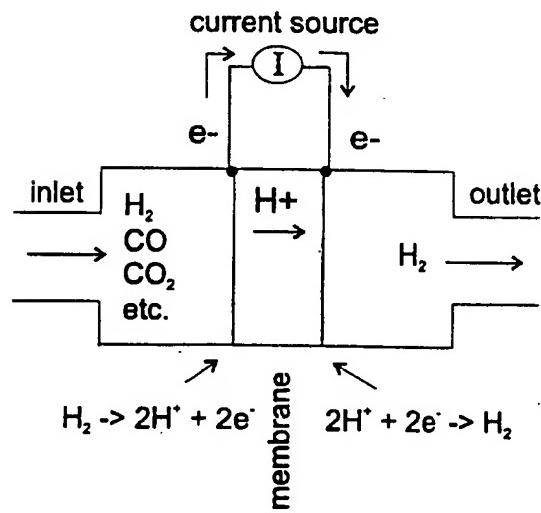
Fig. 3 H₂ Separation Membrane type 1Fig. 4 H₂ Separation Membrane type 2

Fig. 5 Membrane Reactor type 1

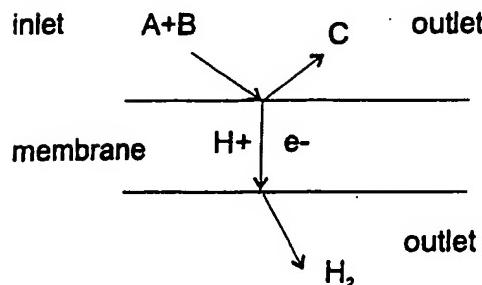
yield enhancementselective hydrogenation.

Fig. 6 Membrane Reactor type 2

